

SOLKANE® - INFORMATION SERVICE

Solkane® 134a

Thermodynamics

SOLVAY FLUOR GMBH

Technical Service - Refrigerants -

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1 Units and Symbols

Symbol	Unit	Meaning/Definition
A, B	[-]	parameters of the Wagner equation
C	[-]	parameter of the equation for density of boiling liquid
D	[kJ/(kg K)]	parameter of the equation for specific heat capacity in an ideal gas state
E, F, G	[-]	parameter of the Martin-Hou equation
H	[Pa s /K]	parameter of the equation for dynamic viscosity
J	[W/(m K)]	parameter of the equation for thermal conductivity of the saturated liquid
L	[W/(m K)]	parameter of the equation for thermal conductivity of the saturated vapour
K	[N/(m K)]	parameter of the equation for surface tension
M	[kJ/(kg K)]	parameter of the equation for specific heat capacity of the saturated liquid
R	[bar m ³ /(kg K)]	gas constant
b	[m ³ /kg]	parameter of the Martin-Hou equation
c	[kJ/(kg K)]	specific heat capacity
e	[kJ/kg]	specific exergy
h	[kJ/kg]	specific enthalpy
k	[-]	parameter of the Martin-Hou equation
p	[bar]	pressure
r	[kJ/kg]	enthalpy of vaporization
s	[kJ/(kg K)]	specific entropy
t	[°C]	temperature
T	[K]	temperature
v	[m ³ /kg]	specific volume
η	[Pa s]	dynamic viscosity
λ	[W/(m K)]	thermal conductivity
ρ	[kg/m ³]	density
σ	[N/m]	surface tension

Indices

$\dot{}$	liquid
$\ddot{}$	vapour
c	critical value
R	reduced value
i	run index
u	ambient conditions
p	isobar
v	isochor
0	ideal gas

2 Introduction

The refrigerant Solkane®134a is a long term replacement for the chlorofluorocarbon (CFC) R12. Solkane®134a ($\text{CF}_3\text{-CH}_2\text{F}$) has the chemical designation 1,1,1,2-tetrafluoroethane and is an isomer of R134 (see section 2.1). The physical and thermodynamic properties of Solkane®134a are very similar to those of R12. In the AFEAS programme (Alternative Fluorocarbon Environmental Acceptability Study), a study jointly financed by a series of different companies, the influence of various partly-halogenated fluorohydrocarbons (HFC) on the environment was assessed - among others Solkane®134a. According to the results, Solkane 134a has no ozone depletion potential (ODP) and has around 90% less direct influence on the greenhouse effect than R12.

Between 1987 and 1992, Solkane®134a was subjected to an intensive toxicological research programme, which was carried out within the scope of PAFT (Programme for Alternative Fluorocarbon Toxicity Testing). Based on the results, Solkane®134a was toxicologically classified as being similar to R12. The TLV for an eight hour working day is estimated as 1000 ppm. The environmental tolerance and handling of Solkane refrigerants is described in the environmental compatibility brochure¹ and material safety data sheet¹.

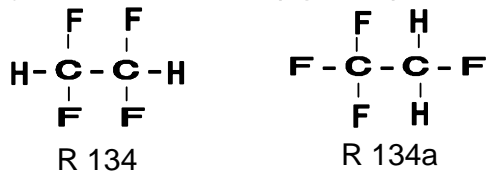
Solkane®134a is non-combustible, demonstrates good material compatibility and possesses good thermal and chemical stability.

¹ Order by fax : 0511/857-2178

2.1 Definition of Isomers

A few refrigerants have an additional lower case letter next to the R-number in accordance with the ASHRAE nomenclature (eg R134a = 1,1,1,2-tetrafluoroethane). This letter serves to distinguish between the different isomers. Two types of isomerism among refrigerants are significant: position isomerism and chain isomerism.

Examples of position isomerism are R134a (1,1,1,2-tetrafluoroethane) and R134 (1,1,2,2-tetrafluoroethane). Refrigerant R134, because of its physical properties, is not a suitable substitute for R12. The boiling points of R134a and R134 are -26.3°C and -19.8 C respectively. The difference is due to the position of the four fluorine (F) and two hydrogen (H) atoms on the carbon (C) centres. The isomers all have the same ASHRAE number. The letters a, b, c, etc. are appended to the number to indicate the degree of asymmetry. (c would be more asymmetrical than b etc.) The most symmetrical isomers (eg R134) are not indicated by a lower case letter.



The difference in the position of the fluorine and hydrogen atoms on the two carbon atom centres can be seen in the structural formulae above.

3 Thermophysical Values

3.1 Physical Data

Chemical name	[-]	1,1,1,2-tetrafluoroethane
Chemical formula	[-]	CH ₂ FCF ₃
Chemical structure	[-]	<pre> F H F — C — C — F F H </pre>
CAS No.	[-]	811-97-2
Molecular weight	[kg/kmol]	102.0
Boiling point ¹	[°C]	-26.06
Freezing point ¹	[°C]	-101
Critical temperature	[°C]	101.1
Critical pressure	[bar]	40.59
Saturated liquid density ²	[kg/m ³]	1206
Saturated vapour density ^{1,2}	[kg/m ³]	32.35
Vapour pressure ^{1,2}	[bar]	6.654
Enthalpy of vaporization ²	[kJ/kg]	177.5
Liquid thermal conductivity ²	[W/m K]	83.51E-3
Vapour thermal conductivity ²	[W/m K]	13.97E-3
Surface tension of liquid ²	[N/m]	8.02E-3
Specific heat capacity of liquid ²	[kJ/(kgK)]	1.425
Specific heat capacity of vapour ^{1,2}	[kJ/(kgK)]	1.011
Liquid viscosity ²	[Pa s]	0.1974E-3
Saturated vapour viscosity ²	[Pa s]	0.01193E-3
Flammability limit in air ¹	[Vol.-%]	none ³

¹ at 1.013 bar

² at 25°C

³ according to DIN 51649 and UL 2128

3.2 Basis of Thermodynamic Calculation

The thermodynamic calculation equations have been adapted to ISO/DIS 17584, as at 12/2003. They fulfil this standard with the exception of the thermal capacities in a saturated state of $0.60 < T_R < 0.96$ and in an overheated state of $0.05\text{MPa} < p < 2.5\text{MPa}$ and $T_{\text{max}} = 500\text{K}$.

The Wagner equation

$$\ln p_R = \left(A_1(1-T_R) + A_2(1-T_R)^{B_1} + A_3(1-T_R)^{B_2} + A_4(1-T_R)^{B_3} + A_5(1-T_R)^{B_4} + A_6 \right) / T_R \quad (1)$$

where $T_R = \frac{T}{T_c}$ and $p_R = \frac{p}{p_c}$

was chosen to describe the vapour pressure. The constants and values for the critical pressure p_c and the critical temperature T_c are as follows:

A_1	[-]	-7.7069E+00	B_1	[-]	1.5158
A_2	[-]	2.4932E+00	B_2	[-]	1.9907
A_3	[-]	-2.9212E+00	B_3	[-]	4.3798
A_4	[-]	-3.8684E+00	B_4	[-]	1.7461
A_5	[-]	4.6898E-01	T_c	[K]	374.21
A_6	[-]	-8.3360E-05	p_c	[bar]	40.59

The density of the boiling liquid is described by the equation

$$\rho'_R = 1 + C_1(1-T_R)^{1/3} + C_2(1-T_R)^{2/3} + C_3(1-T_R) + C_4(1-T_R)^{4/3} \quad (2)$$

where $\rho'_R = \frac{\rho'}{\rho_c}$

The constants and the value for the critical density are:

C_1	[-]	1.732277	C_4	[-]	1.056144
C_2	[-]	1.348322	ρ_c	[kg/m ³]	511.90
C_3	[-]	-1.251446			

The specific heat capacity under ideal gas conditions is represented by the equation

$$c_p^0 = D_1 + D_2T + D_3T^2 + D_4T^3 + D_5/T \quad (3)$$

The coefficients are:

D_1	[kJ/(kg K)]	2.49202E-01	D_3	[kJ/(kg K ³)]	-1.65650E-06
D_2	[kJ/(kg K ²)]	2.45251E-03	D_4	[kJ/kg]	8.91048E-10
D_5	[kJ/kg]	-6.96764E+00			

The equation of state according to Martin-Hou is

$$p = \frac{RT}{z} + \frac{E_1 + F_1T + G_1e^{-kT_R}}{z^2} + \frac{E_2 + F_2T + G_2e^{-kT_R}}{z^3} + \frac{E_3}{z^4} + \frac{E_4 + F_4T + G_4e^{-kT_R}}{z^5} \quad (4)$$

where $z = v - b$

and is a good representation of the pvT relationship for Solkane 134a. The coefficients of the equation are:

E_1	[-]	-1.40114E-03	F_2	[-]	-2.78860E-09
E_2	[-]	2.19433E-06	F_4	[-]	1.02574E-14
E_3	[-]	-6.73580E-10	G_1	[-]	-2.69555E-02
E_4	[-]	-4.66800E-12	G_2	[-]	2.67772E-05
F_1	[-]	1.63714E-06	G_4	[-]	1.69513E-10
b	[m ³ /kg]	2.99628E-04	K	[-]	5.475
R	[bar m ³ /(kg K)]	8.14892E-04			

The equation for specific heat capacity under ideal gas conditions (3) and the thermal equation of state (4) form the basis of the specific enthalpy and entropy calculation. Applying generally valid thermodynamic relationships the equation is transformed to

$$h = h_0 + (pv - RT) + D_1T + D_2\frac{T^2}{2} + D_3\frac{T^3}{3} + D_4\ln T + \frac{E_1}{z} + \frac{E_2}{2z^2} + \frac{E_3}{3z^3} + \frac{E_4}{4z^4} + e^{-k \cdot T_R} \cdot (1 + k \cdot T_R) \cdot \left(\frac{G_1}{z} + \frac{G_2}{2z^2} + \frac{G_4}{4z^4} \right) \quad (5)$$

and

$$s = s_0 + R \ln \left(\frac{zp_1}{RT} \right) + D_1 \cdot \ln T + D_2T + D_3\frac{T^2}{2} - \frac{D_4}{T} - \left(\frac{F_1}{z} + \frac{F_2}{2z^2} + \frac{F_4}{4z^4} \right) + \frac{k}{T_c} e^{-k \cdot T_R} \left(\frac{G_1}{z} + \frac{G_2}{2z^2} + \frac{G_4}{4z^4} \right) \quad (6)$$

where $z = v - b$ and $p_1 = 1.013$ bar.

The Clausius - Clapeyron equation was used to generate thermodynamic data in the wet vapour range.

$$\frac{dp}{dT} = \frac{1}{T} \cdot \frac{h'' - h'}{v'' - v'} \quad (7)$$

Rearranging equation (7) gives

$$h' = h'' - \frac{dp}{dT} \cdot T \cdot (v'' - v') \quad (8)$$

The integration constants h_0 and s_0 are found by letting

$$h'_{(t=0\text{ }^\circ\text{C})} = 200.0 \text{ kJ/kg}$$

$$s'_{(t=0\text{ }^\circ\text{C})} = 1.000 \text{ kJ/(kgK)}$$

to be

$$h_0 = 295.57 \text{ kJ/kg}$$

$$s_0 = -0.2037 \text{ kJ/(kg K)}$$

If neither the kinetic nor the potential energies are taken into account, the specific exergy may be found by the following equation:

$$e = h - h_u - T_u(s - s_u) \quad (9)$$

where the subscript u indicates ambient conditions.

The saturation pressure of the substance at $T_u = 290 \text{ K}$ serves as the reference pressure.

Applying the preconditions mentioned above, the constants h_u and s_u are found to be as follows:

$$h_u = 223.17 \text{ kJ/kg}$$

$$s_u = 1.081 \text{ kJ/(kg K)}$$

3.3 Transport Properties

3.3.1 Dynamic Viscosity of Saturated Liquid

The viscosity of the saturated liquid of Solkane 134a was measured within the temperature range -50 to 60 °C. The following regression equation is valid for the liquid phase:

$$\ln\left(\frac{\eta'}{10^{-3}}\right) = H_0 + H_1t + H_2t^2 + H_3t^3 \quad (10)$$

t is in °C and η' in 10^{-3} Pa s. The coefficients are:

$H_0 =$	-1.29909	[Pa s]	$H_2 =$	4.9223×10^{-6}	[Pa s/K ²]
$H_1 =$	-0.0129286	[Pa s/K]	$H_3 =$	-1.9860×10^{-7}	[Pa s/K ³]

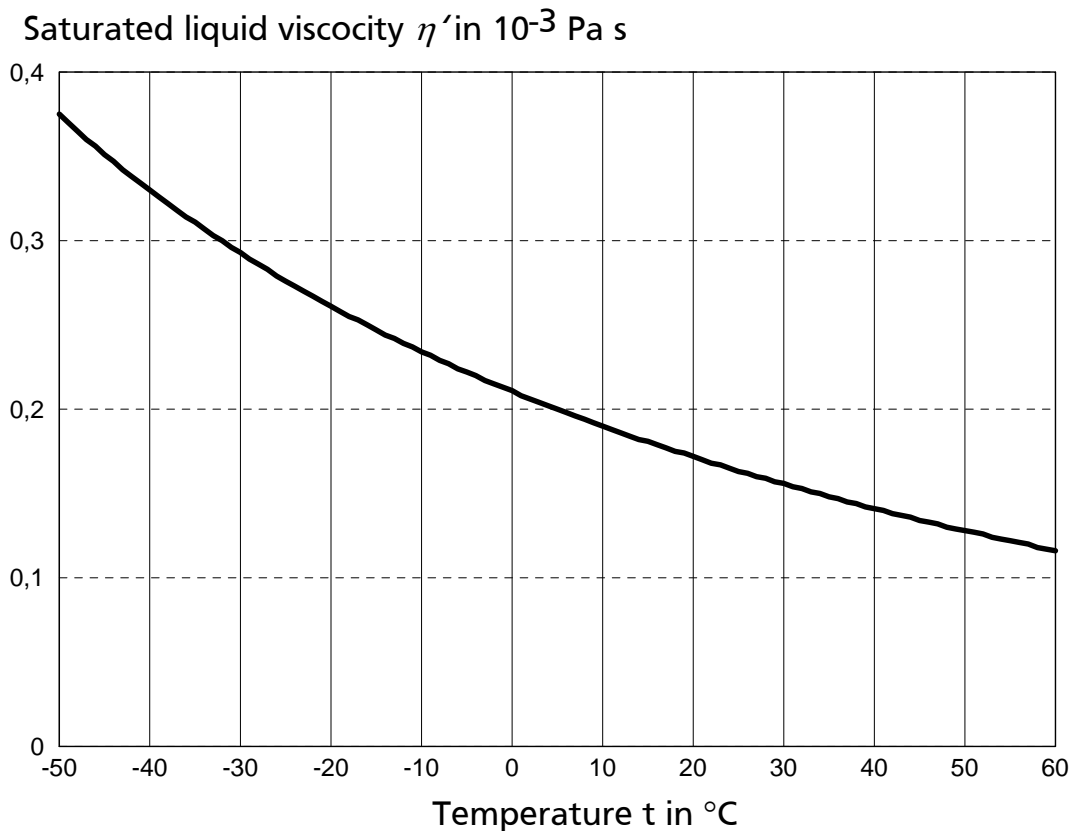


Figure 1: Dynamic saturated liquid viscosity

3.3.2 Dynamic Viscosity of Saturated and Superheated Vapour

The viscosity of the saturated and superheated vapour of Solkane®134a was measured in a temperature range of -50 to 50°C. The data can be represented by the following equations

$$\eta = \eta_0 + \Delta\eta \quad (11)$$

with

$$\eta_0 = 2.6696 \times 10^{-2} \times \frac{(MT)^{\frac{1}{2}}}{\sigma^2 \Omega_\eta T^*}, \quad T^* = \frac{kT}{\varepsilon} \text{ and}$$

$$\Omega(T^*) = \exp[0.45667 - 0.53955(\ln(T^*)) + 0.187265(\ln T^*)^2 - 0.03629(\ln T^*)^3 + 0.00241(\ln T^*)^4] \quad (12 \text{ a-c})$$

$$\Delta\eta = T_R^{2.2} \left[\ln(1.65 + \rho_{R0}^{0.8}) \right]^{1.6} \left[e^{\left(1 - \frac{0.78}{T_c}\right) \rho_{R0}} - 1 \right] (F \cdot z_c \cdot \zeta)^{-1}$$

$$z_c = \frac{p_c V_c}{RT_c} \quad \text{and} \quad \rho_{R0} = \frac{\rho - \rho_0}{\rho_c} \quad \text{and} \quad F = 1 \text{ for R134a as a light polar agent.} \quad (12 \text{ d-f})$$

In equation (12) the constants are as follows:

R the universal gas constant	= 8314	[J kmol ⁻¹ K ⁻¹]
ρ_c the critical density	= 515.30	[kg/m ³]
ρ_0 the density at 1.013bar and temperature as defined by T		[kg/m ³]
T_c the critical temperature	= 374.205	[K]

The constants of equation (11) were determined to be

$$\begin{aligned} \zeta &= 39721 \text{ [1/(Pa s)]} \\ \sigma &= 0.5067 \text{ [nm]} \\ \varepsilon/k &= 277.74 \text{ [K]} \end{aligned}$$

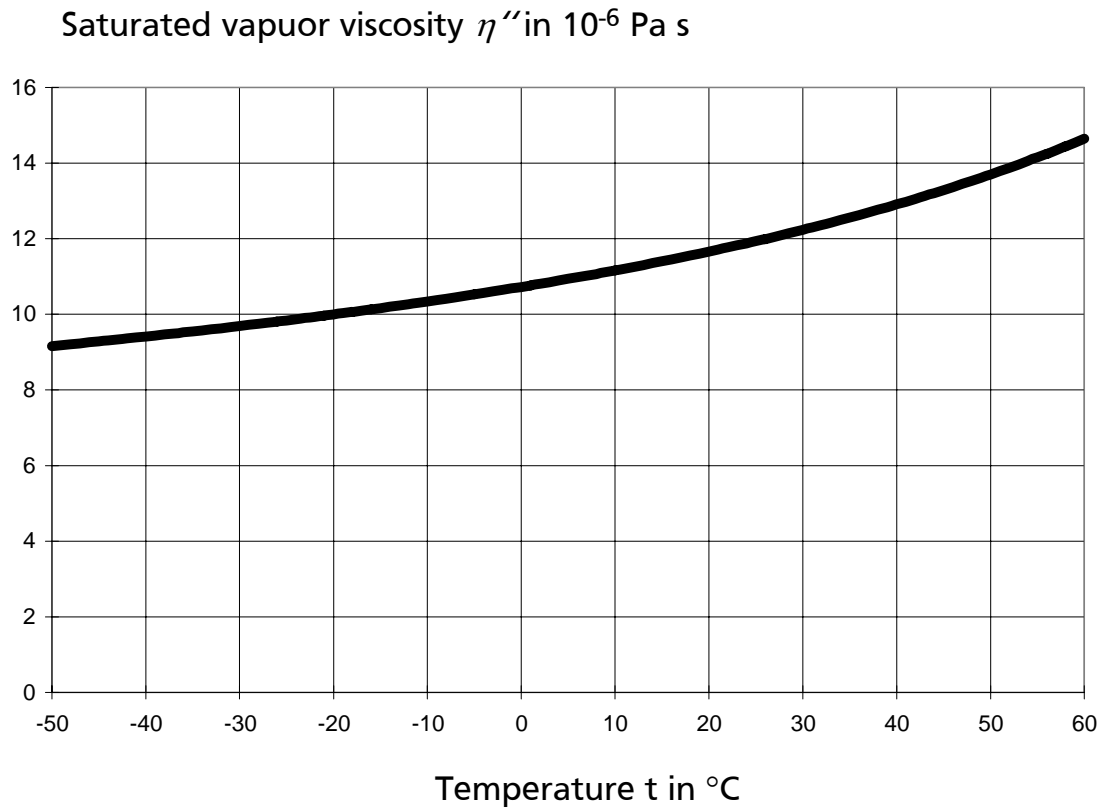


Figure 2: Dynamic viscosity of saturated vapour

3.3.3 Thermal Conductivity of Saturated Liquid

The thermal conductivity of saturated liquid can be expressed with the regression equation

$$\lambda' = J_0 + J_1 t \quad (13)$$

where t is in $^{\circ}\text{C}$ and λ' in $10^{-3} \text{ W}/(\text{mK})$. The coefficients of the equation are:

$$J_0 = 94.21 \quad [10^{-3} \text{ W}/(\text{m K})] \quad J_1 = -0.42784 \quad [10^{-3} \text{ W}/(\text{m K}^2)]$$

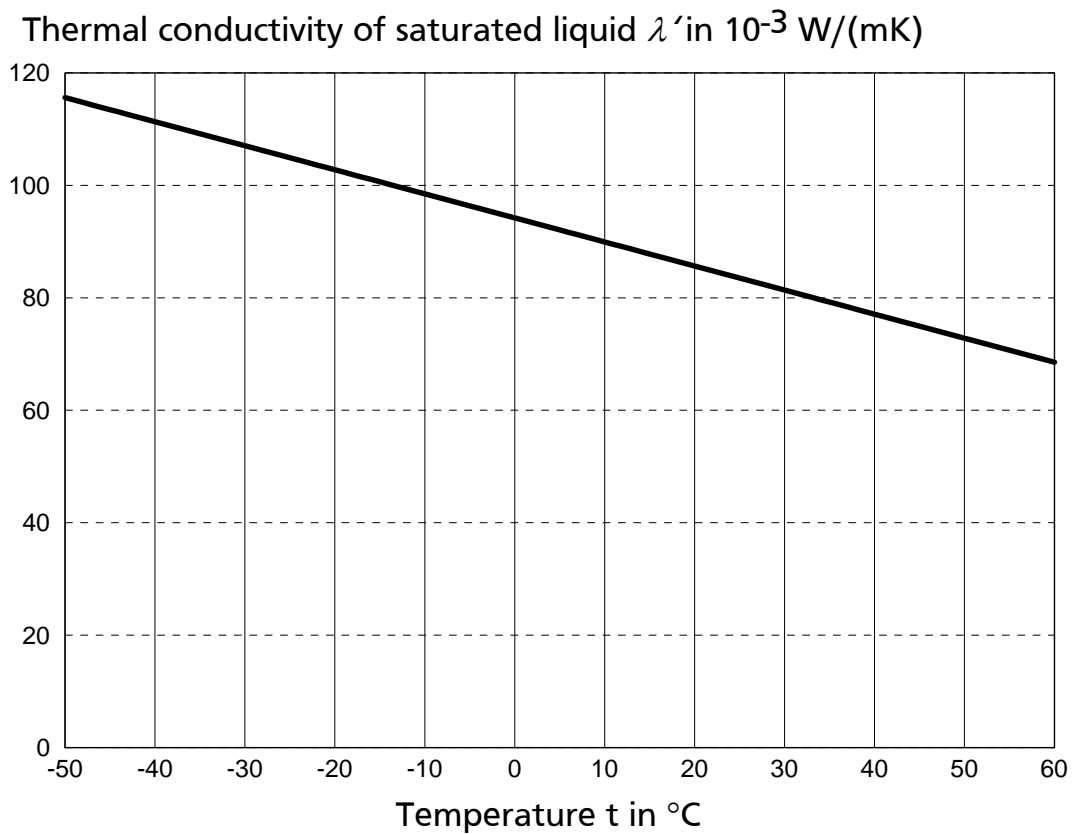


Figure 3: Thermal Conductivity of Saturated Liquid

3.3.4 Thermal Conductivity of Saturated Vapour

The thermal conductivity of saturated vapour can be expressed using the regression equation

$$\lambda'' = L_0 + L_1 t + L_2 t^2 \quad (14)$$

where t is in $^{\circ}\text{C}$ and λ'' in $10^{-3} \text{ W}/(\text{m K})$. The coefficients of the equation are as follows:

$$\begin{aligned} L_0 &= 11.804 && [10^{-3} \text{ W}/(\text{m K})] \\ L_1 &= 0.0805 && [10^{-3} \text{ W}/(\text{m K}^2)] \\ L_2 &= 1.33741 \times 10^{-4} && [10^{-3} \text{ W}/(\text{m K}^3)] \end{aligned}$$

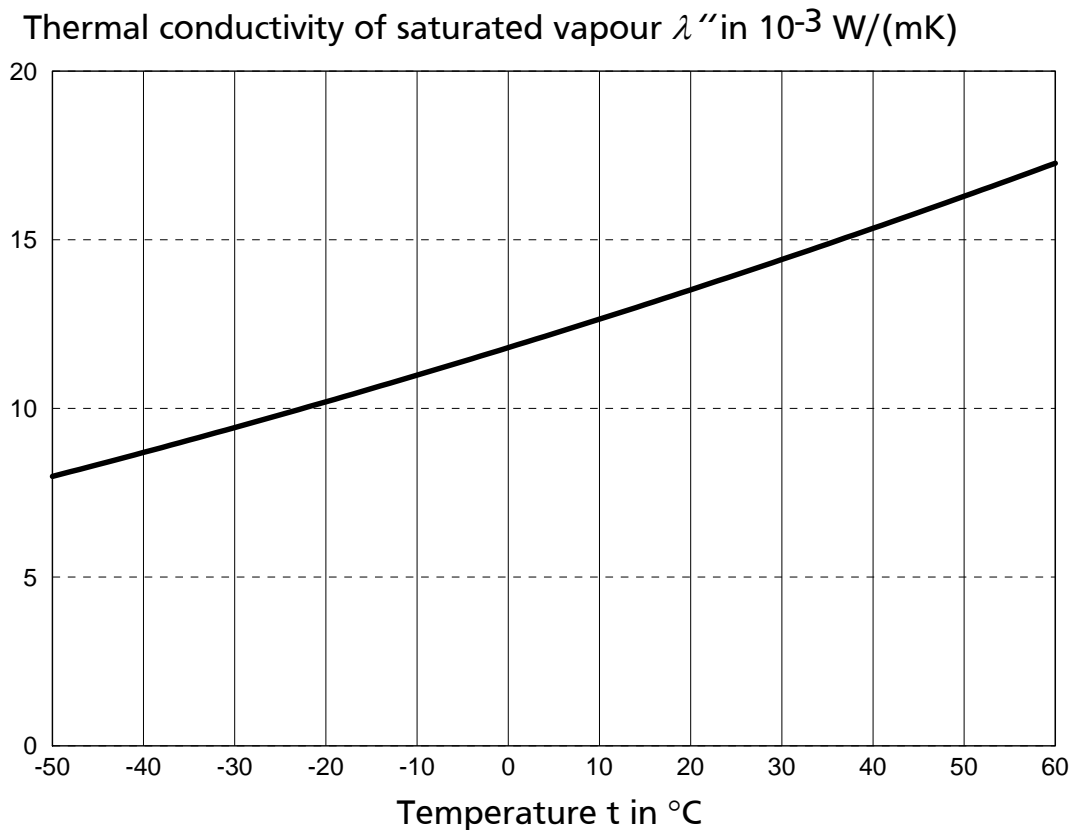


Figure 4: Thermal conductivity of saturated vapour

3.3.5 Surface Tension

The surface tension of the liquid can be expressed using the regression equation

$$\sigma = K_0 + K_1 t + K_2 t^2 + K_3 t^3 \quad (15)$$

where t is in °C und σ in 10^{-3} N/m. The coefficients of the equation are:

$$\begin{aligned} K_0 &= 11.4860 [10^{-3} \text{ N/m}] & K_2 &= 1.3133 \times 10^{-4} [10^{-3} \text{ N/(mK}^2\text{)}] \\ K_1 &= -0.14267 [10^{-3} \text{ N/(mK)}] & K_3 &= 1.1697 \times 10^{-6} [10^{-3} \text{ N/(mK}^3\text{)}] \end{aligned}$$

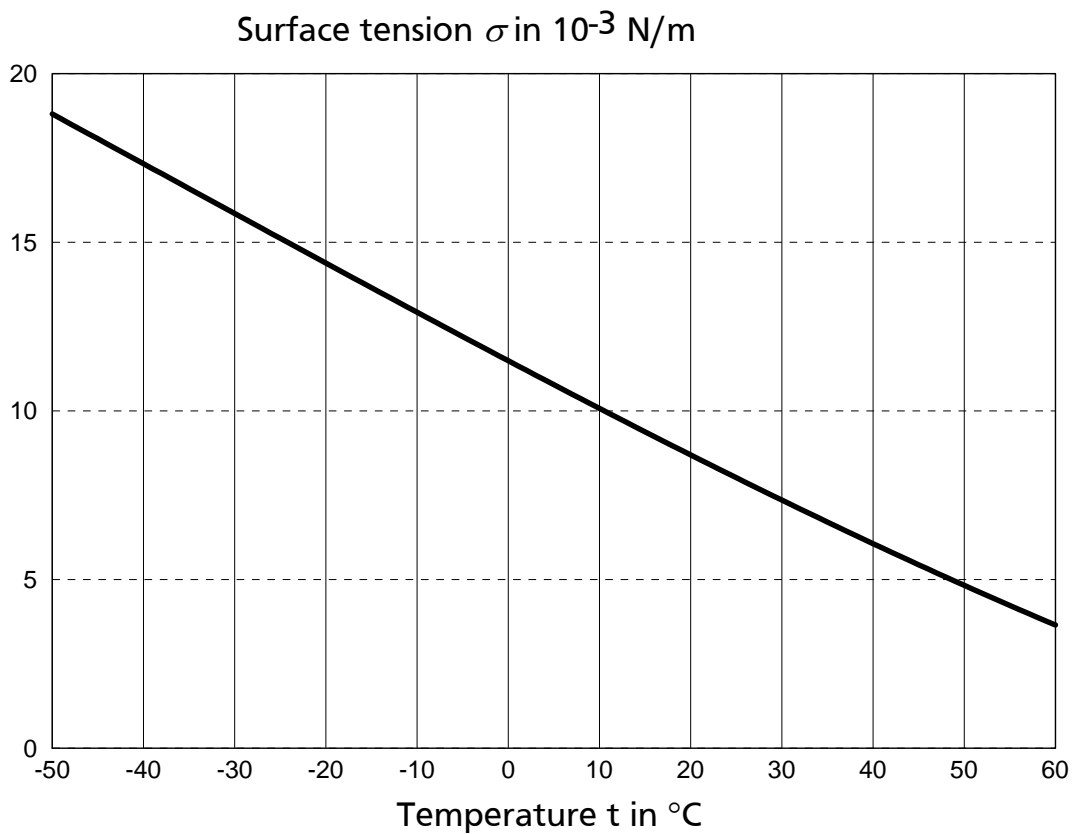


Figure 5: Surface tension

3.3.6 Specific Heat Capacity of Saturated Liquid

The specific heat capacity of saturated fluid can be expressed using the equation

$$c'_p = M_0 + M_1(1 - T_R)^{1/9} + M_2(1 - T_R)^{2/9} + M_3(1 - T_R)^{3/9} + M_4(1 - T_R)^{6/9} \quad (16)$$

where $T_R = \frac{T}{T_c}$, c'_p is in kJ/(kg K) and T is in K. The coefficients of the equation are as follows:

$M_0 = 395.19033$ [kJ/(kg K)]	$M_3 = -1120.361$ [kJ/(kg K)]
$M_1 = -1588.637$ [kJ/(kg K)]	$M_4 = 81.256634$ [kJ/(kg K)]
$M_2 = 2233.8111$ [kJ/(kg K)]	$T_c = 374.205$ [K]

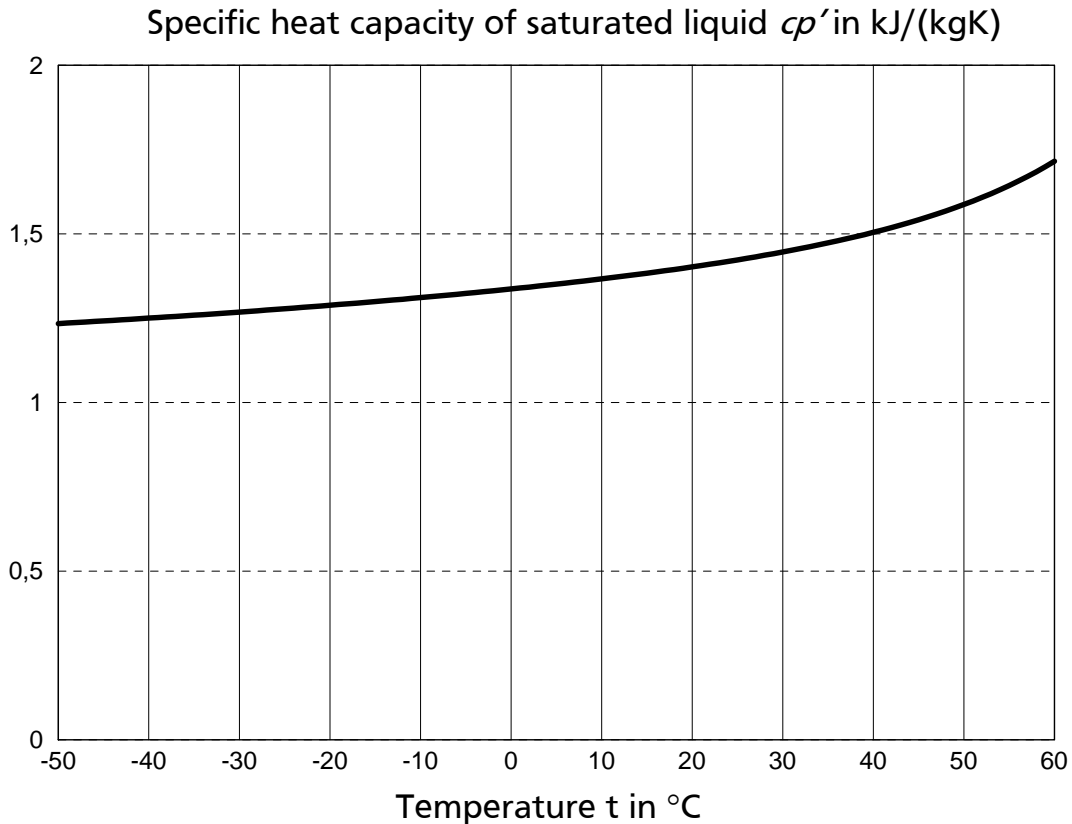


Figure 6: Specific heat capacity of saturated liquid

4 Compatibility of Materials

4.1 Elastomeres

The compatibility of materials with Solkane®134a was checked according to DIN 8944 using various selected elastomers. The extraction tests, which were carried out on the elastomers usually used in refrigeration technology CR, NBR and H-NBR, showed only slight swelling and yielded negligible amounts of extract. Fluorinated rubbers (types FKM and FPM) are not recommended because of their considerable swelling and blistering when used with Solkane®134a. Ethylenepropylenediene rubber is only to be recommended where the presence of mineral oil in the refrigeration cycle can be excluded. The effect of the lubricant which is used must not be ignored. Recommendations made by the lubricant and compressor manufacturers must be followed.

Table 1: Cold extraction tests according to DIN 8944: Solkane®134a

Elastomer		Change in weight [%]	Extract [%]
IIR	butyl rubber	-1.1	0
EPDM	ethylenepropylenediene rubber	-0.4	0
HNBR	hydrated acrylonitrilebutadiene rubber	-0.11	0
CR	chlorobutadiene rubber (Neoprene)	-0.15	0
NBR	acrylonitrilebutadiene rubber	-0.29	0
NR	natural rubber	-0.6	0
FKM	fluoro rubber	+7.3	0.1

Sample post treatment: 1h drying at 50°C

Extract post treatment: 24h drying at 100°C

4.2 Thermoplastics

Experience with CFC and H-CFC has shown that only a limited number of plastics are resistant to fluorinated refrigerants. Various plastics used in refrigeration technology were stored for 50 days at room temperature. It is vital to take the possible additional effect of the lubricants into account. The following table of values can only be used to give an idea of the effects to be expected.

Tabelle 2: Storage tests for Solkane®134a and Thermoplastics

Thermoplast	Change in weight /%			Optical changes ¹	
	Drying time:	-	1 h		24 h
Hostaform S 27076		10.3	9.5	6.1	0
Hostaform S 9064		2.7	2.5	1.6	0
Hostaform C 9021 GV		0.8	0.8	0.4	0
Fortron 6165 A4 natural		0	0	0	0
Fortron 1140 L4 natural		-0.1	-0.1	-0.1	0
Hostalit Z		-0.1	-0.1	-0.1	0
Polyethylene GM 7746		0.6	0.5	0.3	0
Polyethylene GA 7260		0.5	0.4	0.2	++
Polystyrene 4000		0.5	0.3	0.1	+
Polystyrene 6600		0.8	0.7	0.4	0
Vectra A 130 + 30% Glass fibres		-0.1	-0.1	-0.1	0
Vectra C 130 + 30% Glass fibres		-0.1	-0.1	-0.1	0
Vectra A 530 + 30% Mineral content		-0.1	-0.1	-0.1	0
Vectra C 810		0	0	0	0
Vectra C 510		0	0	0	0
Polypropylene PPX 4207		0.9	0.9	0.5	0
Polypropylene PPW 1752		0.7	0.7	0.4	0
Polypropylene PPN 1060		0.5	0.4	0.3	0

¹ 0 : no change, + surface attacked, ++ surface delaminated

4.3 Metals

Solkane®134a is generally used in conjunction with lubricants (Ester oils, PAG-oils) in refrigeration technology. The combination of both these materials is compatible with the metals and joints usually found in machines and apparatus. Only zinc, magnesium, lead and aluminium alloys with more than 2% magnesium by mass should be avoided. The water content of refrigeration oil depending on oil type should especially be taken into account. Values of not more than 50 ppm are to be aimed at.

5 Refrigerant Oils

Like all fluorinated hydrocarbons, Solkane®134a is immiscible with mineral oils. Ester oil, and in automotive airconditioning systems, fully synthetic polyglycols (PAG) are used as lubricants. The solubility of these oils in Solkane®134a is a function of temperature and composition. The following diagram shows the solubility properties of various lubricants with Solkane®134a. Highly viscous lubricants tend to give large miscibility gaps.

The precise miscibility gaps of the individual oils can be obtained from the lubricant manufacturers.

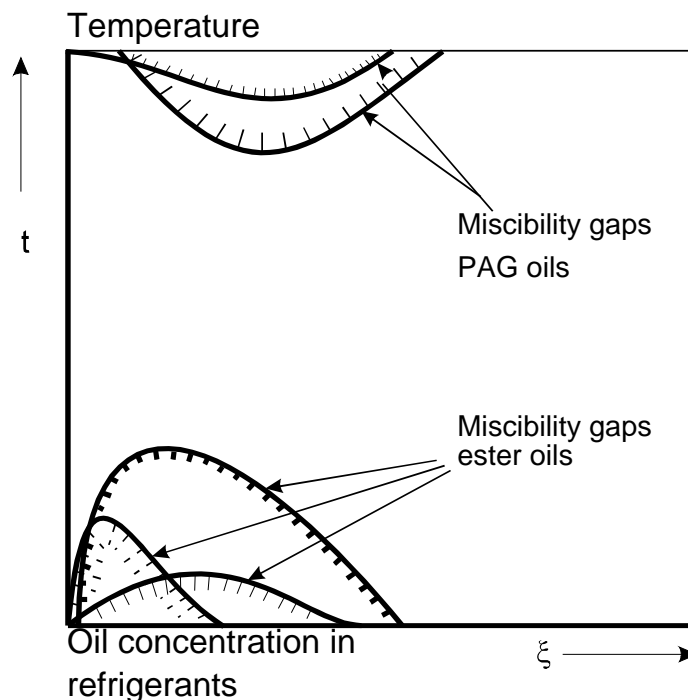


Figure 7: An example of a depiction of miscibility gaps from different types of synthetic lubricants.

6 Thermal Stability

Solkane®134a demonstrates a better thermal stability than the CFCs which have been used up to now. No fluoride ions were found by the Phillip test in accordance with DIN 51 593 (refrigerant + mineral oil in a U-tube for 96 h at 250°C). The product has therefore passed the Phillip test.

7 Flammability

According to DIN 51649 and UL 2182 Solkane®134a is non-flammable.

8 Toxicity

The toxicity of Solkane®134a was extensively tested between 1987 and 1994 within the scope of the PAFT programme (Programme for Alternative Fluorocarbon Toxicity Testing). The tests showed that the safety for Solkane®134a with regard to toxicity was at least as high as that for R12. The results showed that the product can be safely used in domestic, commercial and industrial refrigeration and in air conditioning technology. The usual measures which are recommended for work safety must be followed. Solvay recommends a TLV of 1000 ppm.

9 Vapour Table, Wet Vapour Range Solkane®134a

t	p'	v'	v''	ρ'	ρ''	h'	h''	r	s'	s''
[°C]	[bar]	[dm ³ /kg]	[dm ³ /kg]	[kg/dm ³]	[kg/m ³]	[kJ/kg]	[kJ/kg]	[kJ/kg]	[kJ/kgK]	[kJ/kgK]
-50	0.29	0.691	606.17	1.447	1.65	135.75	367.70	231.95	0.7409	1.7808
-49	0.31	0.692	574.14	1.444	1.74	136.99	368.33	231.34	0.7463	1.7790
-48	0.33	0.694	544.11	1.441	1.84	138.24	368.96	230.73	0.7518	1.7772
-47	0.35	0.695	515.95	1.438	1.94	139.49	369.60	230.11	0.7572	1.7755
-46	0.37	0.697	489.51	1.436	2.04	140.73	370.23	229.50	0.7626	1.7738
-45	0.39	0.698	464.68	1.433	2.15	141.98	370.86	228.89	0.7681	1.7722
-44	0.41	0.699	441.35	1.430	2.27	143.22	371.50	228.27	0.7735	1.7706
-43	0.44	0.701	419.41	1.427	2.38	144.47	372.13	227.66	0.7789	1.7690
-42	0.46	0.702	398.76	1.424	2.51	145.71	372.76	227.05	0.7842	1.7674
-41	0.49	0.704	379.33	1.421	2.64	146.96	373.39	226.43	0.7896	1.7659
-40	0.51	0.705	361.01	1.418	2.77	148.21	374.02	225.81	0.7950	1.7645
-39	0.54	0.706	343.76	1.415	2.91	149.46	374.66	225.20	0.8003	1.7630
-38	0.57	0.708	327.49	1.413	3.05	150.71	375.29	224.58	0.8057	1.7616
-37	0.60	0.709	312.13	1.410	3.20	151.96	375.92	223.95	0.8110	1.7602
-36	0.63	0.711	297.64	1.407	3.36	153.21	376.54	223.33	0.8163	1.7589
-35	0.66	0.712	283.95	1.404	3.52	154.47	377.17	222.70	0.8217	1.7576
-34	0.70	0.714	271.01	1.401	3.69	155.73	377.80	222.08	0.8270	1.7563
-33	0.73	0.715	258.78	1.398	3.86	156.98	378.43	221.45	0.8322	1.7551
-32	0.77	0.717	247.20	1.395	4.05	158.24	379.06	220.81	0.8375	1.7538
-31	0.80	0.718	236.25	1.392	4.23	159.51	379.68	220.18	0.8428	1.7526
-30	0.84	0.720	225.88	1.389	4.43	160.77	380.31	219.54	0.8480	1.7515
-29	0.88	0.721	216.05	1.386	4.63	162.04	380.93	218.89	0.8533	1.7503
-28	0.93	0.723	206.73	1.383	4.84	163.31	381.56	218.25	0.8585	1.7492
-27	0.97	0.725	197.90	1.380	5.05	164.58	382.18	217.60	0.8637	1.7481
-26	1.02	0.726	189.51	1.377	5.28	165.85	382.80	216.94	0.8689	1.7471
-25	1.06	0.728	181.56	1.374	5.51	167.13	383.42	216.29	0.8741	1.7460
-24	1.11	0.729	174.00	1.371	5.75	168.41	384.04	215.63	0.8793	1.7450
-23	1.16	0.731	166.82	1.368	5.99	169.69	384.66	214.96	0.8845	1.7440
-22	1.22	0.733	160.00	1.365	6.25	170.98	385.28	214.30	0.8896	1.7431
-21	1.27	0.734	153.51	1.362	6.51	172.27	385.89	213.62	0.8948	1.7421
-20	1.33	0.736	147.33	1.359	6.79	173.56	386.51	212.95	0.8999	1.7412
-19	1.39	0.738	141.46	1.356	7.07	174.85	387.12	212.27	0.9050	1.7403
-18	1.45	0.739	135.86	1.353	7.36	176.15	387.73	211.58	0.9101	1.7394
-17	1.51	0.741	130.54	1.349	7.66	177.45	388.34	210.90	0.9152	1.7385
-16	1.57	0.743	125.46	1.346	7.97	178.75	388.95	210.20	0.9203	1.7377
-15	1.64	0.744	120.62	1.343	8.29	180.06	389.56	209.51	0.9254	1.7369
-14	1.71	0.746	116.00	1.340	8.62	181.36	390.17	208.81	0.9304	1.7361
-13	1.78	0.748	111.60	1.337	8.96	182.68	390.77	208.10	0.9355	1.7353
-12	1.85	0.750	107.39	1.334	9.31	183.99	391.38	207.39	0.9405	1.7346
-11	1.93	0.752	103.38	1.331	9.67	185.31	391.98	206.67	0.9455	1.7338

Vapour Table, Wet Vapour Range Solkane®134a

t	p'	v'	v''	ρ'	ρ''	h'	h''	r	s'	s''
[°C]	[bar]	[dm ³ /kg]	[dm ³ /kg]	[kg/dm ³]	[kg/m ³]	[kJ/kg]	[kJ/kg]	[kJ/kg]	[kJ/kgK]	[kJ/kgK]
-10	2.01	0.753	99.54	1.327	10.05	186.63	392.58	205.95	0.9505	1.7331
-9	2.09	0.755	95.88	1.324	10.43	187.95	393.18	205.23	0.9555	1.7324
-8	2.17	0.757	92.38	1.321	10.82	189.28	393.78	204.50	0.9605	1.7317
-7	2.25	0.759	89.03	1.318	11.23	190.61	394.37	203.77	0.9655	1.7310
-6	2.34	0.761	85.83	1.315	11.65	191.94	394.97	203.03	0.9705	1.7304
-5	2.43	0.763	82.76	1.311	12.08	193.27	395.56	202.29	0.9754	1.7297
-4	2.53	0.765	79.83	1.308	12.53	194.61	396.15	201.54	0.9804	1.7291
-3	2.62	0.766	77.02	1.305	12.98	195.95	396.74	200.79	0.9853	1.7285
-2	2.72	0.768	74.33	1.301	13.45	197.30	397.32	200.03	0.9902	1.7279
-1	2.82	0.770	71.75	1.298	13.94	198.64	397.91	199.27	0.9951	1.7273
0	2.93	0.772	69.28	1.295	14.43	200.00	398.49	198.49	1.0000	1.7267
1	3.04	0.774	66.91	1.291	14.95	201.35	399.07	197.72	1.0049	1.7262
2	3.15	0.776	64.64	1.288	15.47	202.70	399.65	196.95	1.0098	1.7256
3	3.26	0.778	62.46	1.285	16.01	204.06	400.22	196.16	1.0146	1.7251
4	3.38	0.780	60.36	1.281	16.57	205.42	400.80	195.38	1.0195	1.7246
5	3.50	0.782	58.35	1.278	17.14	206.79	401.37	194.58	1.0243	1.7241
6	3.62	0.785	56.42	1.275	17.72	208.15	401.94	193.78	1.0292	1.7236
7	3.75	0.787	54.57	1.271	18.33	209.52	402.50	192.98	1.0340	1.7231
8	3.88	0.789	52.79	1.268	18.94	210.90	403.07	192.17	1.0388	1.7226
9	4.01	0.791	51.08	1.264	19.58	212.27	403.63	191.36	1.0436	1.7221
10	4.15	0.793	49.43	1.261	20.23	213.65	404.19	190.54	1.0484	1.7217
11	4.29	0.795	47.84	1.257	20.90	215.03	404.74	189.71	1.0532	1.7212
12	4.43	0.798	46.32	1.254	21.59	216.42	405.30	188.88	1.0580	1.7208
13	4.58	0.800	44.85	1.250	22.29	217.80	405.85	188.04	1.0627	1.7204
14	4.73	0.802	43.44	1.247	23.02	219.19	406.39	187.20	1.0675	1.7200
15	4.88	0.804	42.08	1.243	23.76	220.58	406.94	186.35	1.0723	1.7196
16	5.04	0.807	40.77	1.240	24.53	221.98	407.48	185.50	1.0770	1.7192
17	5.21	0.809	39.51	1.236	25.31	223.38	408.02	184.64	1.0818	1.7188
18	5.37	0.811	38.30	1.232	26.11	224.78	408.55	183.77	1.0865	1.7184
19	5.54	0.814	37.12	1.229	26.94	226.18	409.08	182.90	1.0912	1.7180
20	5.72	0.816	35.99	1.225	27.78	227.59	409.61	182.02	1.0960	1.7176
21	5.90	0.819	34.91	1.221	28.65	229.00	410.14	181.14	1.1007	1.7172
22	6.08	0.821	33.85	1.218	29.54	230.41	410.66	180.25	1.1054	1.7169
23	6.27	0.824	32.84	1.214	30.45	231.83	411.18	179.35	1.1101	1.7165
24	6.46	0.826	31.86	1.210	31.39	233.25	411.69	178.44	1.1148	1.7162
25	6.65	0.829	30.91	1.206	32.35	234.67	412.20	177.53	1.1195	1.7158
26	6.85	0.832	30.00	1.202	33.33	236.09	412.71	176.61	1.1242	1.7155
27	7.06	0.834	29.12	1.199	34.34	237.52	413.21	175.69	1.1289	1.7151
28	7.27	0.837	28.27	1.195	35.38	238.96	413.71	174.75	1.1336	1.7148
29	7.48	0.840	27.44	1.191	36.44	240.39	414.20	173.81	1.1383	1.7144

Vapour Table, Wet Vapour Range Solkane®134a

t	p'	v'	v''	ρ'	ρ''	h'	h''	r	s'	s''
[°C]	[bar]	[dm ³ /kg]	[dm ³ /kg]	[kg/dm ³]	[kg/m ³]	[kJ/kg]	[kJ/kg]	[kJ/kg]	[kJ/kgK]	[kJ/kgK]
30	7.70	0.842	26.65	1.187	37.53	241.83	414.69	172.86	1.1429	1.7141
31	7.93	0.845	25.88	1.183	38.64	243.27	415.18	171.91	1.1476	1.7138
32	8.15	0.848	25.13	1.179	39.79	244.72	415.66	170.94	1.1523	1.7134
33	8.39	0.851	24.41	1.175	40.96	246.17	416.14	169.97	1.1570	1.7131
34	8.63	0.854	23.72	1.171	42.16	247.62	416.61	168.99	1.1616	1.7128
35	8.87	0.857	23.04	1.167	43.40	249.08	417.07	168.00	1.1663	1.7124
36	9.12	0.860	22.39	1.163	44.66	250.54	417.54	167.00	1.1710	1.7121
37	9.37	0.863	21.76	1.159	45.96	252.01	417.99	165.99	1.1757	1.7118
38	9.63	0.866	21.15	1.155	47.29	253.48	418.44	164.97	1.1804	1.7114
39	9.90	0.869	20.55	1.150	48.66	254.95	418.89	163.94	1.1850	1.7111
40	10.17	0.872	19.98	1.146	50.06	256.43	419.33	162.90	1.1897	1.7107
41	10.44	0.876	19.42	1.142	51.49	257.91	419.76	161.85	1.1944	1.7104
42	10.72	0.879	18.88	1.138	52.97	259.40	420.19	160.79	1.1991	1.7100
43	11.01	0.882	18.36	1.133	54.48	260.90	420.61	159.72	1.2038	1.7097
44	11.30	0.886	17.85	1.129	56.03	262.40	421.03	158.63	1.2085	1.7093
45	11.60	0.889	17.36	1.125	57.62	263.90	421.44	157.54	1.2132	1.7090
46	11.90	0.893	16.88	1.120	59.25	265.41	421.84	156.43	1.2179	1.7086
47	12.21	0.896	16.41	1.116	60.92	266.93	422.24	155.31	1.2226	1.7082
48	12.53	0.900	15.96	1.111	62.64	268.45	422.63	154.17	1.2273	1.7078
49	12.85	0.904	15.53	1.107	64.40	269.98	423.01	153.02	1.2320	1.7075
50	13.18	0.908	15.10	1.102	66.21	271.52	423.38	151.86	1.2367	1.7071
51	13.51	0.911	14.69	1.097	68.07	273.07	423.75	150.68	1.2415	1.7066
52	13.85	0.915	14.29	1.093	69.98	274.62	424.10	149.49	1.2462	1.7062
53	14.20	0.919	13.90	1.088	71.94	276.18	424.45	148.28	1.2510	1.7058
54	14.55	0.923	13.52	1.083	73.95	277.74	424.79	147.05	1.2557	1.7053
55	14.92	0.928	13.15	1.078	76.02	279.32	425.12	145.81	1.2605	1.7049
56	15.28	0.932	12.80	1.073	78.15	280.90	425.44	144.54	1.2653	1.7044
57	15.66	0.936	12.45	1.068	80.34	282.49	425.76	143.26	1.2701	1.7039
58	16.04	0.941	12.11	1.063	82.59	284.10	426.06	141.96	1.2749	1.7034
59	16.42	0.945	11.78	1.058	84.90	285.71	426.35	140.64	1.2797	1.7029
60	16.82	0.950	11.46	1.053	87.28	287.33	426.63	139.30	1.2845	1.7024
61	17.22	0.955	11.15	1.047	89.72	288.96	426.90	137.94	1.2894	1.7018
62	17.63	0.960	10.84	1.042	92.24	290.60	427.15	136.55	1.2942	1.7012
63	18.04	0.965	10.54	1.037	94.84	292.26	427.40	135.14	1.2991	1.7006
64	18.47	0.970	10.26	1.031	97.51	293.92	427.63	133.71	1.3040	1.7000
65	18.90	0.975	9.97	1.026	100.27	295.60	427.84	132.25	1.3089	1.6994
66	19.34	0.980	9.70	1.020	103.11	297.29	428.05	130.76	1.3138	1.6987
67	19.78	0.986	9.43	1.014	106.04	298.99	428.24	129.25	1.3188	1.6980
68	20.24	0.992	9.17	1.008	109.06	300.71	428.41	127.70	1.3237	1.6973
69	20.70	0.998	8.91	1.002	112.19	302.44	428.57	126.13	1.3287	1.6965

Vapour Table, Wet Vapour Range Solkane®134a

t	p'	v'	v''	ρ'	ρ''	h'	h''	r	s'	s''
[°C]	[bar]	[dm ³ /kg]	[dm ³ /kg]	[kg/dm ³]	[kg/m ³]	[kJ/kg]	[kJ/kg]	[kJ/kg]	[kJ/kgK]	[kJ/kgK]
70	21.17	1.004	8.66	0.996	115.41	304.18	428.71	124.52	1.3337	1.6957
71	21.65	1.010	8.42	0.990	118.75	305.94	428.83	122.88	1.3387	1.6949
72	22.13	1.016	8.18	0.984	122.20	307.72	428.93	121.21	1.3438	1.6940
73	22.63	1.023	7.95	0.978	125.77	309.51	429.01	119.50	1.3489	1.6931
74	23.13	1.030	7.72	0.971	129.47	311.32	429.07	117.76	1.3539	1.6921
75	23.64	1.037	7.50	0.964	133.30	313.14	429.11	115.97	1.3590	1.6911
76	24.16	1.044	7.28	0.958	137.28	314.99	429.13	114.14	1.3642	1.6901
77	24.69	1.052	7.07	0.951	141.42	316.85	429.12	112.27	1.3693	1.6890
78	25.23	1.060	6.86	0.944	145.71	318.73	429.08	110.35	1.3745	1.6878
79	25.78	1.068	6.66	0.936	150.19	320.64	429.02	108.38	1.3797	1.6866
80	26.33	1.077	6.46	0.929	154.85	322.56	428.93	106.37	1.3850	1.6852
81	26.90	1.086	6.26	0.921	159.71	324.50	428.80	104.30	1.3903	1.6839
82	27.47	1.095	6.07	0.913	164.79	326.47	428.64	102.17	1.3955	1.6824
83	28.06	1.105	5.88	0.905	170.11	328.46	428.44	99.98	1.4009	1.6809
84	28.65	1.116	5.69	0.896	175.69	330.47	428.19	97.72	1.4062	1.6792
85	29.26	1.127	5.51	0.888	181.54	332.51	427.91	95.40	1.4116	1.6775
86	29.87	1.138	5.33	0.879	187.71	334.57	427.57	93.01	1.4170	1.6756
87	30.50	1.151	5.15	0.869	194.22	336.66	427.19	90.53	1.4225	1.6736
88	31.14	1.164	4.97	0.859	201.11	338.77	426.74	87.97	1.4280	1.6715
89	31.78	1.178	4.80	0.849	208.42	340.91	426.23	85.31	1.4335	1.6692
90	32.44	1.193	4.63	0.838	216.21	343.08	425.64	82.56	1.4391	1.6667
91	33.11	1.210	4.45	0.827	224.56	345.28	424.97	79.69	1.4447	1.6641
92	33.79	1.228	4.28	0.814	233.54	347.52	424.20	76.69	1.4503	1.6611
93	34.49	1.248	4.11	0.801	243.26	349.78	423.33	73.55	1.4560	1.6579
94	35.19	1.270	3.94	0.788	253.90	352.07	422.31	70.24	1.4617	1.6544
95	35.91	1.295	3.76	0.772	265.66	354.40	421.13	66.73	1.4675	1.6504
96	36.64	1.324	3.59	0.755	278.91	356.76	419.73	62.96	1.4733	1.6459
97	37.39	1.358	3.40	0.736	294.32	359.16	417.99	58.84	1.4791	1.6405

Vapour Table, Superheated Range Solkane® 134a

1.708bar -14°C					2.169bar -8°C					2.722bar -2°C					3.377bar 4°C				
t	v	h	s		t	v	h	s		t	v	h	s		t	v	h	s	
°C	dm ³ /kg	kJ/kg	kJ/kgK		°C	dm ³ /kg	kJ/kg	kJ/kgK		°C	dm ³ /kg	kJ/kg	kJ/kgK		°C	dm ³ /kg	kJ/kg	kJ/kgK	
-14	116.00	390.17	1.7361		-8	92.38	393.78	1.7317		-2	74.33	397.32	1.7279		4	60.36	400.80	1.7246	
-10	118.26	393.48	1.7488		-5	93.76	396.33	1.7412		0	75.09	399.07	1.7343		5	60.68	401.70	1.7278	
-5	121.05	397.63	1.7644		0	96.02	400.58	1.7570		5	76.96	403.44	1.7502		10	62.24	406.19	1.7438	
0	123.81	401.80	1.7798		5	98.26	404.86	1.7725		10	78.79	407.83	1.7658		15	63.78	410.69	1.7596	
5	126.54	406.00	1.7951		10	100.46	409.15	1.7878		15	80.60	412.22	1.7812		20	65.28	415.20	1.7751	
10	129.24	410.23	1.8101		15	102.64	413.47	1.8029		20	82.39	416.64	1.7964		25	66.77	419.72	1.7904	
15	131.92	414.49	1.8250		20	104.80	417.82	1.8179		25	84.15	421.08	1.8114		30	68.23	424.26	1.8055	
20	134.58	418.77	1.8398		25	106.93	422.19	1.8326		30	85.89	425.53	1.8262		35	69.67	428.81	1.8204	
25	137.21	423.09	1.8544		30	109.05	426.58	1.8473		35	87.62	430.01	1.8409		40	71.10	433.38	1.8351	
30	139.83	427.44	1.8688		35	111.15	431.01	1.8617		40	89.33	434.52	1.8554		45	72.50	437.97	1.8496	
35	142.44	431.82	1.8832		40	113.24	435.47	1.8761		45	91.02	439.06	1.8697		50	73.90	442.59	1.8640	
40	145.02	436.24	1.8974		45	115.31	439.95	1.8903		50	92.70	443.62	1.8840		55	75.28	447.23	1.8783	
45	147.60	440.69	1.9115		50	117.37	444.47	1.9044		55	94.37	448.21	1.8981		60	76.66	451.90	1.8924	
50	150.16	445.17	1.9255		55	119.41	449.02	1.9184		60	96.03	452.83	1.9120		65	78.02	455.59	1.9064	
55	152.71	449.69	1.9394		60	121.45	453.61	1.9322		65	97.68	457.49	1.9259		70	79.37	461.32	1.9203	
60	155.26	454.25	1.9531		65	123.48	458.23	1.9460		70	99.32	462.17	1.9397		75	80.71	466.07	1.9340	
65	157.79	458.84	1.9668		70	125.50	462.88	1.9597		75	100.95	466.89	1.9533		80	82.05	470.86	1.9477	

1.852bar -12°C					2.343bar -6°C					2.928bar 0°C					3.620bar 6°C				
t	v	h	s		t	v	h	s		t	v	h	s		t	v	h	s	
°C	dm ³ /kg	kJ/kg	kJ/kgK		°C	dm ³ /kg	kJ/kg	kJ/kgK		°C	dm ³ /kg	kJ/kg	kJ/kgK		°C	dm ³ /kg	kJ/kg	kJ/kgK	
-12	107.39	391.38	1.7346		-6	85.83	394.97	1.7304		0	69.28	398.49	1.7267		6	56.42	401.94	1.7236	
-10	108.45	393.05	1.7409		-5	86.26	395.82	1.7336		5	71.05	402.90	1.7427		10	57.61	405.57	1.7365	
-5	111.06	397.22	1.7566		0	88.39	400.11	1.7494		10	72.79	407.32	1.7585		15	59.07	410.11	1.7524	
0	113.64	401.42	1.7722		5	90.49	404.42	1.7650		15	74.49	411.75	1.7740		20	60.50	414.66	1.7680	
5	116.18	405.65	1.7875		10	92.56	408.74	1.7804		20	76.18	416.19	1.7893		25	61.91	419.21	1.7834	
10	118.70	409.90	1.8026		15	94.60	413.08	1.7956		25	77.84	420.65	1.8044		30	63.29	423.77	1.7986	
15	121.20	414.17	1.8176		20	96.63	417.45	1.8107		30	79.48	425.13	1.8193		35	64.65	428.35	1.8136	
20	123.67	418.48	1.8324		25	98.62	421.84	1.8255		35	81.10	429.64	1.8340		40	66.00	432.95	1.8284	
25	126.12	422.81	1.8471		30	100.60	426.26	1.8402		40	82.70	434.16	1.8486		45	67.33	437.56	1.8430	
30	128.56	427.17	1.8616		35	102.57	430.70	1.8547		45	84.30	438.72	1.8630		50	68.65	442.20	1.8575	
35	130.98	431.57	1.8760		40	104.52	435.17	1.8691		50	85.87	443.30	1.8773		55	69.95	446.86	1.8718	
40	133.38	436.00	1.8902		45	106.45	439.67	1.8834		55	87.44	447.90	1.8914		60	71.24	451.55	1.8860	
45	135.77	440.46	1.9043		50	108.37	444.21	1.8975		60	88.99	452.54	1.9054		65	72.53	456.26	1.9000	
50	138.15	444.95	1.9184		55	110.28	448.77	1.9115		65	90.54	457.21	1.9193		70	73.80	461.00	1.9139	
55	140.52	449.48	1.9323		60	112.18	453.37	1.9254		70	92.07	461.90	1.9331		75	75.06	465.77	1.9277	
60	142.87	454.05	1.9461		65	114.07	458.00	1.9392		75	93.60	466.63	1.9468		80	76.32	470.57	1.9414	
65	145.22	458.65	1.9598		70	115.95	462.66	1.9529		80	95.12	471.39	1.9604		85	77.56	475.39	1.9550	

2.006bar -10°C					2.527bar -4°C					3.146bar 2°C					3.876bar 8°C				
t	v	h	s		t	v	h	s		t	v	h	s		t	v	h	s	
°C	dm ³ /kg	kJ/kg	kJ/kgK		°C	dm ³ /kg	kJ/kg	kJ/kgK		°C	dm ³ /kg	kJ/kg	kJ/kgK		°C	dm ³ /kg	kJ/kg	kJ/kgK	
-10	99.54	392.58	1.7331		-4	79.83	396.15	1.7291		2	64.64	399.65	1.7256		8	52.79	403.07	1.7226	
-5	101.99	396.79	1.7489		0	81.44	399.61	1.7419		5	65.64	402.32	1.7353		10	53.35	404.90	1.7291	
0	104.41	401.02	1.7646		5	83.41	403.95	1.7576		10	67.29	406.78	1.7512		15	54.74	409.49	1.7452	
5	106.79	405.27	1.7800		10	85.36	408.30	1.7731		15	68.90	411.24	1.7668		20	56.10	414.07	1.7609	
10	109.14	409.54	1.7952		15	87.28	412.67	1.7884		20	70.49	415.71	1.7822		25	57.44	418.66	1.7765	
15	111.47	413.83	1.8102		20	89.18	417.06	1.8035		25	72.06	420.20	1.7974		30	58.75	423.26	1.7918	
20	113.78	418.16	1.8251		25	91.06	421.47	1.8184		30	73.61	424.71	1.8124		35	60.05	427.87	1.8068	
25	116.07	422.51	1.8398		30	92.91	425.91	1.8332		35	75.14	429.24	1.8272		40	61.32	432.49	1.8217	
30	118.33	426.89	1.8544		35	94.75	430.37	1.8478		40	76.65	433.78	1.8418		45	62.58	437.13	1.8364	
35	120.59	431.30	1.8688		40	96.57	434.86	1.8622		45	78.14	438.36	1.8563		50	63.82	441.79	1.8509	
40	122.82	435.74	1.8831		45	98.38	439.37	1.8765		50	79.62	442.95	1.8706		55	65.05	446.47	1.8653	
45	125.05	440.21	1.8973		50	100.18	443.92	1.8907		55	81.09	447.58	1.8848		60	66.27	451.18	1.8795	
50	127.26	444.72	1.9113		55	101.96	448.50	1.9048		60	82.55	452.23	1.8989		65	67.48	455.90	1.8936	
55	129.46	449.26	1.9253		60	103.73	453.11	1.9187		65	84.00	456.91	1.9128		70	68.68	460.66	1.9076	
60	131.64	453.84	1.9391		65	105.50	457.75	1.9325		70	85.44	461.62	1.9267		75	69.87	465.44	1.9214	
65	133.82	458.44	1.9529		70	107.25	462.42	1.9463		75	86.87	466.36	1.9404		80	71.05	470.25	1.9352	
70	136.00	463.09	1.9665		75	109.00	467.13	1.9599		80	88.30	471.13	1.9540		85	72.23	475.10	1.9498	

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